

# Reciprocating plate column – fundamental research and application in Serbia from 1970 to 2020

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Table S-1. Types of RPCs [1]

Plate type	Reciprocating element	Characteristics	Country
Karr (KRPC)	Plates with large openings (open type)	Column diameter up to 1.7 m Large fractional free plate surface (50-60 %) Large plate opening diameter (10-16 mm) Plate modification – with a central opening (Baird type) Inserted buffers along the column of larger diameter reduce the radial flow non-uniformity. Operating mode: homogeneous	USA, Canada, Western Europe, India, Serbia
Prochazka (PRPC)	Plates with downcomers or segmental passages	Column diameter up to 1.2 m Small fractional free plate surface (4-30 %) Small plate opening diameter (2-5 mm) With a drain in the form of a pipe or a segmental passage in the form of a cut-off part of the plate (free surface fraction of 10-25 %) Movement of plats: all in the same phase or every other with a phase shift of 180° Operating mode: segregated and homogeneous	Czech Republic, Canada
Tojo and Miyanami (VDC)	Vibrating discs	Discs without perforations The fractional free plate surface depends on the disk diameter-to-column diameter ratio (4-0.78 %) Static buffers between every two disks	Japan
Karpačeva and Gorodetskiy (KRIMZ, GIAP)	Plates with rectangular openings	Column diameter up to 1.5 m, height up to 11 m Fractional-free plate surface about 45 % Rectangular openings with bent ends that divert fluid flow radially to reduce axial mixing Plates without (KRIMZ) or with a drain (GIAP)	Former USSR

<sup>a</sup>GIAP – the plate with rectangular openings with a drain, KRIMZ – the plate with rectangular openings without a drain, KRPC – the Karr type RPC, PRPC – the Prochazka type RPC, and VDC – the vibrating disc column.

Table S-2. Overview of previous research on RPCs in Serbia (adapted according to [1])

System	Phase flow	$D_c$ / cm	$l_c$ / m	$n_p$	$h$ / cm	$d_o$ / cm	$\varepsilon$	$A$ / mm	$f$ / Hz	$u_g$ / cm s <sup>-1</sup>	Subject <sup>a</sup>	Ref.
Water	-	2.54		18			0.51				$\Delta p, P$	[2]
Water-toluene, water- <i>n</i> -butanol	Batch	2.54	2.11	78	2.54	0.8	0.51	5-19.6	0.5-3.5	-	$\Delta p, P$	[3]
Water-toluene	-	2.54	2.71	18	2.54	ND	0.51	20.5	0.275-2	-	$\Delta p$	[4]
Water, air-sulfite solution	↑↓	2.54	2.14	65	2.6	0.8/0.6	0.51	0.65-2	0.483-6.18	0.8-3.2	$D_i, \varepsilon_g, a$	[5]
Air-water	↑↓	2.54	2.14	32 64	2.54 5.08	0.8/0.6	0.51	0.65-1.5	1.83-6	0.8; 2.9	$D_i$	[6]
Water, air-sucrose solution	↑↓	2.54	2	33 65	2.54	0.7/0.5 0.8/0.6	0.41 0.51	<10 and <20	<10	< 5	$\Delta p, P, \varepsilon_g, k\alpha, a$	[7]



System	Phase flow	$D_c$ /cm	$l_c$ /m	$n_p$	$h$ /cm	$d_o$ /cm	$\varepsilon$	$A$ /mm	$f$ /Hz	$u_g$ /cm s <sup>-1</sup>	Subject <sup>a</sup>	Ref.
Water, air-sucrose, sulfate, mixtures of sucrose, fructose, and dextran	↑↓	2.54	2.14	32 64	2.54 5.08	0.8/0.6	0.51	0.65–1.5	1.83–6	0.275 to 1.1	$k_1a$ , dextran sucrose production	[8]
Water, air-sucrose, air-water	Batch	2.54	2	65 33	2.5 5.0	0.7/0.5	0.41	1–10	1–10	0.275 to 2.75	$\Delta p, P, \varepsilon_g$	[9]
Air-water	↑↓	2.54	2	33 65	5.0 2.5	0.7/0.5	0.41	1–10	1–10		$\varepsilon_g$	[10]
Water, air-solutions of sucrose, sulfate, and mixtures of sucrose, fructose, and dextran	↑↓	2.54	2	65 33	5.08 2.54	0.8/0.6 0.7/0.5	0.51 0.41	<20	<6.2	<5	$k_1a$	[11]
Water, air, N <sub>2</sub> , O <sub>2</sub> -sucrose and sulfite solutions	Batch or ↑↓	2.54	2	65 33	5.08 2.54	0.8/0.6	0.51	<20	<6.2	<5	$a$	[12]
Air-water	↑↓	2.54	2	65 32	2.54 5.08	0.8/0.6	0.51	0–20	0–6.25	0.8–3.1	$\varepsilon_g$	[13]
Water, air-sucrose solution, fermentation medium	↑↓	2.54	2	65 33	2.54 5.08	0.8/0.6 0.7/0.5	0.51 0.41	-	-	-	$k_1a$ , dextran sucrose production	[14]
Air-water-solid	↑↓	2.54	2	65	2.54	0.8	0.51	17	0–6.4	0.5–12.8	$\varepsilon_g, d_b$	[15]
Air-water	Batch	2.54	2	65	2.54	0.8/0.6	0.51	13–23.5	1–7.2	0.4–7.5	$\Delta p, P, \varepsilon_g$	[16, 17]
Water, butanol (0.5 %), glycerol (69 %, 64 %), sulfite (0.8 mol dm <sup>-3</sup> ) and CMC (1 and 2 %) solutions; 2-phase (gas-liquid; liquid-solid) and 3-phase systems	Batch	2.54 9.2	1.836 1.05	65 15	2.54 5	0.8 0.8	0.51 0.454	2.35 2.35	2–6 2–6	0.5–1.5 0.5–1.5	$\Delta p, P, \varepsilon_g, d_b, k_1a, a$	[18–20]
Water, air-water, air-water-solid, air-CMC, air-CMC solution (1 %)-solid solution (1 %)-solid	Batch	9.2	1.05	15	5	0.8	0.263 0.319 0.454	2.35	2–6	0.5–1.5	$\Delta p, P, \varepsilon_g, k_1a, a$	[21–26]
CMC solution	Batch	9.2	1.05	15	5	0.8	0.454	2.35	2–5.5	0.5–1.5	$\varepsilon_g$	[27–30]
Air-water-solid	↑↓	2.54 9.2	1.836 0.856	65 15	2.54 5.0	0.8 0.8	0.51 0.454	2.35;1 2.35;1	2–4.5 2–4.5	0–1.48 0–1.88	$D_i, \varepsilon_g$ , alcoholic fermentation	[31–37]
Air-water, air-water-solid	↑↓	16.6	0.97	15	5	0.78	0.466	2.35	2–6	0.5–1.5	$\Delta p, P, \varepsilon_g, k_1a$	[31–37]
Air-CMC solution (0.5 - 1.5 %)-solid	Batch	9.2	1.05	15	5	0.8/0.6	0,454	2.35	2-5,5	0.5–1.5	$\varepsilon_g$	[38–43]
Methanol-oil, methanol-KOH-oil	↑ ↑	2.54	2.0	63	2.54	0.8/0.6	0.51	1.0 2.35	2-5	-	$\Delta p, P, d_b, a$ , biodiesel production	[44]
Methanol-KOH-oil	↑ ↑	2.54 16.6	2.0 1.53	63 15	2.54 5	0.8/0.6 0.8	0.51 0.466	1.0 2.35	2-4 2	-	biodiesel production	[45]
Methanol-oil, methanol-KOH-oil	↑ ↑	2.54	2.0	63	2.54	0.8/0.6	0.51	1.0	2.0	-	$d_b$ , biodiesel production	[46]
Methanol-KOH-waste lard	↑ ↑	2.54	2.0	63	2.54	0.8/0.6	0.51	1.0	2.0	-	Kinetic modeling of biodiesel production	[47]

<sup>a</sup> $a$  – specific interfacial area,  $d_b$  – bubble/drop size,  $D_i$  – axial dispersion coefficient,  $k_1$  – liquid mass transfer coefficient,  $k_1a$  – volumetric mass transfer coefficient,  $\Delta p$  – pressure variation at the column bottom,  $P$  – power consumption,  $\varepsilon_d$  – dispersed phase (methanol) holdup, and  $\varepsilon_g$  – gas holdup.

Table S-3. Worldwide applications of RPCs (adapted according to [1])

Plate type <sup>a</sup>	Application	Reference
KRPC	Copper extraction	[47]
	Lysine biosynthesis	[48]
	Treatment of wastewater	[49]
	Extraction of the product from the fermentation liquid	[50]
	Penicillin extraction	[51]
	Biosynthesis of dextransucrase	[6,3]
	Production of antibiotics, ethanol, and citric acid	[52]
	Fermentation processes	[53]
	Fermentation of pullulan	[54]
	Ester saponification reaction	[55]
	Rare earth separation and recovery	[56]
	Extraction of phenol from water	[57-59]
	Caffeine extraction	[60]
	Alcoholic fermentation with immobilized yeast cells	[33]
	Biodiesel production	[43-46]
Extraction of natural alkaloids	[61]	
PRPC	Production of ephedrine and erythromycin Extraction of phenol and nitro-aromatic derivatives from wastewater	Cited according to [62]
KRIMZ, GIAP	Caprolactam extraction with organic solvents Extraction of cyclohexanone and cyclohexanol with benzene	Cited according to [62]

<sup>a</sup>GIAP – the plate with rectangular openings with a drain, KRIMZ – the plate with rectangular openings without a drain, KRPC – the Karr type plate, and PRPC – the Prochazka type plate.

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